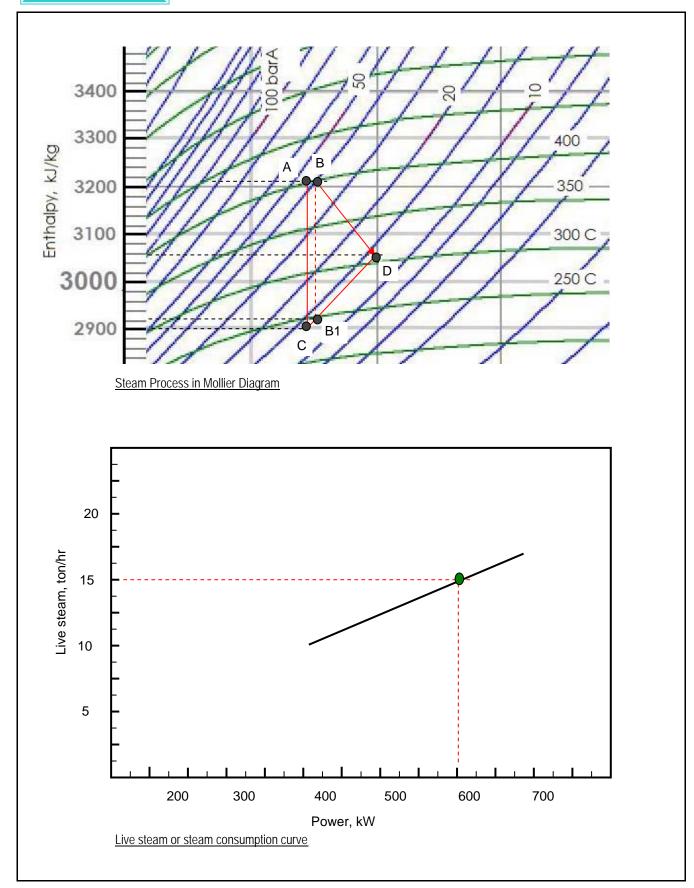


## STEAM TURBINE CALCULATION SHEET

| No.      | Designation                                 |                    | Quantity   |       | Note and additional information                                 |
|----------|---|--------------------|------------|-------|---|
| 1<br>2   | Turbine type, figure 3                      |                    | CUR        | RTIS  |   |
| 3        | 51 - 5                                      |                    | STAND      |       |   |
| 4        | REQUIRED CONDITION                          |                    |            |       |   |
| 5        |   | 1 /l               | Normal     | Rated |   |
| 6<br>7   | Steam flow available, m<br>Turbine speed, N | ton/hr<br>RPM      | 15<br>4000 |       | Pefere reducing gear or without gear                            |
| 8        | Inlet pressure, pi                          | bar A              | 4000       |       | Before reducing gear or without gear                            |
| 9        | Inlet temperature, ti                       | C                  | 400        |       |   |
| 10       | Exhaust pressure, po                        | bar A              | 13         |       |   |
| 11       |   |                    |            |       |   |
| 12       | STEAM DATA                                  |                    |            |       |   |
| 13       | hi  | kJ/kg              | 3210       |       | See steam Mollier diagram, point A                              |
| 14       | hos   | kJ/kg              | 2900       |       | Mollier diagram, isentropic proc., point C                      |
| 15       | Δhs   | kJ/kg              | 310        |       | = hi - hos (point A to C)                                       |
| 16       | Governor valve factor                       |                    | 0.93       |       | Multi valve 0.97, single valve 0.93                             |
| 17       | ∆hs'  | kJ/kg              | 288.3      |       | = Gov. vlv. Factor x $\Delta$ hs (equation 11)                  |
| 18       | hos'  | kJ/kg              | 2921.7     |       | Point B1  |
| 19<br>20 | pi'<br>ti'                                  | bar A              | 39<br>205  |       | Point B for pressure  |
| 20       |   | C<br>3             | 395        |       | Point B for temperature   |
| 21       | vi'   | m <sup>3</sup> /kg | 0.075      |       | See steam table at pi' and ti'                                  |
| 22       | CALCULATION                                 |                    |            |       |   |
| 23       | Nom. Diameter at best eff.,                 | mm                 | 1004       |       | Equation in figure 9. at $\mu$ s = 6.5 (for Curtis)             |
| 24       | Design dia., D                              | mm                 | 1000       |       | Fill with adjustment  |
| 25       | Peripheral velocity, U                      | m/s                | 209.80     |       | Equation 1  |
| 26       | Head coefficient, $\mu_S$                   |                    | 6.550      |       | Equation 4  |
| 27       | Efficiency, $\eta_{05}$                     |                    | 0.71       |       | Figure 12   |
| 28       | Entrance area factor, A                     |                    | 34         |       | Page 16   |
| 29       | 3 X L                                       | mm                 | 0.541      |       | Equation 15 but replace P by ( $\Delta$ hs' x m x $\eta_{05}$ ) |
| 30       | Design nozzle height, I                     | mm                 | 25.0       |       | Fill so that $\boldsymbol{\epsilon}$ within the range below     |
| 31       | Degree of admission, $\epsilon$             |                    | 0.022      |       | Half circle, 0.015-0.45 for wld, min. 0.007 reaming             |
| 32       | Efficiency factor FI                        |                    | 0.95       |       | Figure 13   |
| 33       | Efficiency factor Fe                        |                    | 0.794      |       | Equation in figure 13   |
| 34       | Efficiency, $\eta_1$                        |                    | 0.54       |       | $= \eta_{05} \times F_1 \times F_{\epsilon}$                    |
| 35       | ∆he   | kJ/kg              | 154.4      |       | $= \eta_1 x \Delta hs'$   |
| 36       | he<br>Evhauat tamparatura ta                | kJ/kg              | 3055.6     |       | = hi - $\Delta$ he, point D in Mollier diagram                  |
| 37       | Exhaust temperature, to                     | C<br>3             | 305        |       | See steam Mollier diagram at point D                            |
| 38       | Exhaust specific volume, vo                 | m <sup>3</sup> /kg | 0.19936    |       | See steam table   |
| 39       | P <sub>LOSS</sub>                           | kW                 | 68.49      |       | Equation 5  |
| 40       | Mechanical efficiency, $\eta_m$             |                    | 0.956      |       | Figure 15   |
| 41       | Turbine efficiency, η                       |                    | 0.51       |       | $= \eta_1 X \eta_m$   |
| 42       | Power                                       | kW                 | 546.54     |       | Equation 9  |
| 43       | Note for cell and font color :              |                    |            |       |   |
| 44       | XXX.X Input data or data ta                 |                    |            | XXX.X | Selected data or design where adjustment                        |
| 45       | XXX.X Calculation result or                 |                    | t has been |       | is permitted  |
|          | converted in equatio                        | n                  |            |       |   |







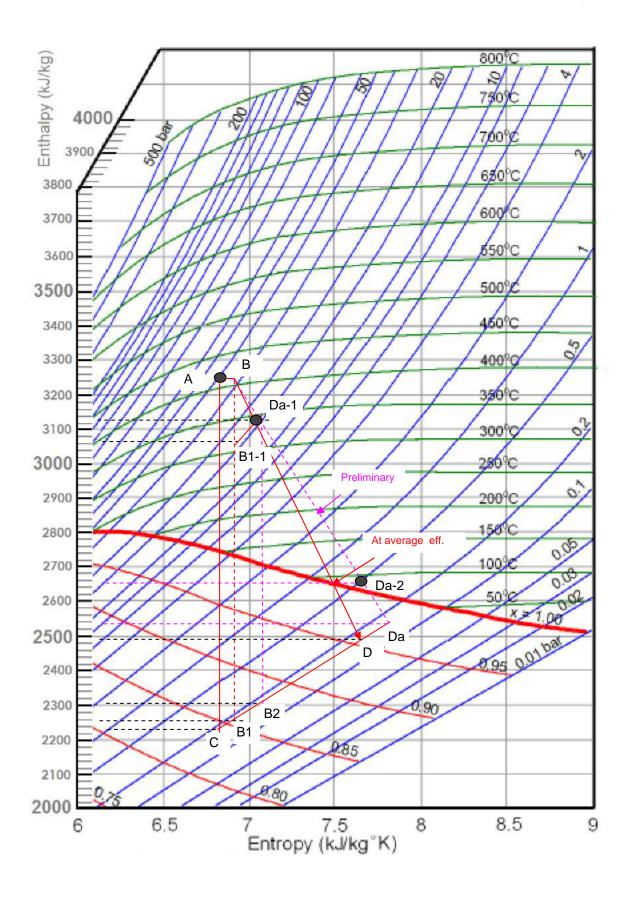
## STEAM TURBINE CALCULATION SHEET

| No.      | Designation                                   |          | Quantity |            | Note and additional information                                 |
|----------|---|----------|----------|------------|---|
| 1        |   |          |          |            |   |
| 2        | Turbine type, figure 3                        |          |          |            |   |
| 3<br>4   | REQUIRED CONDITION                            |          | CONDENSI | NG TURBINE |   |
| 5        | RECORED CONDITION                             |          | Normal   | Rated      |   |
| 6        | Driven equipment                              |          |          | ompressor  |   |
| 7        | Steam flow available                          | ton/hr   | 15       |            |   |
| 8        | Ν   | RPM      | 10200    |            |   |
| 9        | pi  | bar A    | 40       |            |   |
| 10       | ti  | С        | 400      |            |   |
| 11<br>12 | ро<br>Стелм рата                              | bar A    | 0.12     |            |   |
| 12       | <u>STEAM DATA</u><br>hi                       | kJ/kg    | 3205     |            | See steam Mollier diagram, point A                              |
| 14       | hos   | kJ/kg    | 2160     |            | Mollier diagram, isentropic proc., point C                      |
| 15       | Δhs   | kJ/kg    | 1045     |            | = hi - hos  |
| 16       | Governor valve factor                         |          | 0.97     |            | Multi valve 0.97, single valve 0.93                             |
| 17       | ∆hs'  | kJ/kg    | 1013.65  |            | = Gov. vlv. Factor x $\Delta$ hs (equation 11)                  |
| 18       | hos'  | kJ/kg    | 2191.35  |            | Point B1  |
| 19       | pi'   | bar A    | 36       |            |   |
| 20       | ti'   | C<br>3 " | 395      |            | At hi and pi'   |
| 21       | vi'   | m³/kg    | 0.081    |            | See steam table at pi' and ti'                                  |
| 22       |   |          |          |            |   |
| 23       | CALCULATION                                   |          |          |            |   |
| 24<br>25 | Min. no. of stages, zmin<br>Design dia., D    | mm       | 5<br>500 |            | Fig. 10. Nearest cross point RPM vs red dot line                |
| 25       | Calculated number of stages, z1               | 111111   | 6.04     |            | Fig. To. Nearest cross point RPM vs red dot line                |
| 20       | Design no. of stages, z                       |          | 6        |            | Integer   |
| 28       | Enthalpy per stage, $\Delta h_{STG}$          | kJ/kg    | 168.9    |            | $= \Delta hs' / z$  |
| 29       | Peripheral velocity, U                        | m/s      | 267.5    |            | Equation 1  |
| 30       | Head coefficient, $\mu_{S}$                   | 11/5     | 2.36     |            | Equation 4  |
| 31       | Efficiency, $\eta_{05}$                       |          | 0.81     |            | Figure 12   |
|          |   |          |          |            | rigule 12   |
| 32<br>33 | Entrance area factor, A<br><u>First stage</u> |          | 34       |            |   |
| 33<br>34 | <u>  X ε</u>                                  | mm       | 1.527    |            | Equation 15 but replace P by ( $\Delta$ hs' x m x $\eta_{05}$ ) |
| 35       | Nozzle height, I                              | mm       | 25       |            | Fill with adjustment  |
| 36       | Degree of admission, $\varepsilon$            |          | 0.061    |            | Max. 0.9 for Rateau turbine, fig. 16                            |
| 37       | Efficiency factor F <sub>1</sub>              |          | 0.97     |            | Figure 13   |
| 38       | Efficiency factor F                           |          | 0.905    |            | Equation in figure 13   |
| 39       | Efficiency, $\eta_1$                          |          | 0.72     |            | $= \eta_{05} \times F_1 \times F_{\epsilon}$                    |
| 40       | hos <sub>1</sub>                              | kJ/kg    | 3036.06  |            | = hi - $\Delta h_{STG}$ , point B1-1                            |
| 41       | $\Delta he_{STG-1}$                           | kJ/kg    | 120.81   |            | $= \eta_{05} x \Delta h_{STG}$                                  |
| 41       | he <sub>stG-1</sub>                           | kJ/kg    | 3084.19  |            | = $h_{05} \wedge \Delta h_{STG-1}$ , point B1-2                 |
|          |   | 0        | 16.0     |            |   |
| 43       | po <sub>1</sub>                               | bar A    |          |            | See steam chart at point B1-2                                   |
| 44       | to <sub>1</sub>                               | C<br>3   | 325.0    |            |   |
| 45       | VO <sub>1</sub>                               | m³/kg    | 0.167    |            | See steam table   |
| 46       | P <sub>LOSS-1</sub>                           | kW       | 74.42    |            | Equation 5  |
|          |   |          |          |            |   |

| tage<br>reliminary)<br>eliminary)<br>(preliminary)<br>uperheated X for wet steam<br>ce area factor, A<br>height, I<br>hcy factor F <sub>1</sub><br>hcy factor Fε<br>hcy, η <sub>Z</sub> | kJ/kg<br>kJ/kg<br>bar A<br>C for ti<br>m <sup>3</sup> /kg<br>mm<br>mm | 724.9<br>2480.1<br>2600.9<br>0.49<br>0.99<br>3.29<br>43<br>60.238<br>75<br>0.803  | = $\eta_{I} x \Delta hs'$ (preliminary eff. = 1'stg eff.)<br>=hi - $\Delta he$ , point Da<br>=he <sub>Z</sub> + ( $\Delta he/z$ ). Point Da-2<br>Point Da-2<br>See steam table for specific volume<br>Page 16<br>Equation 15 but replace P by ( $\Delta hs' x m x \eta_{05}$ )<br>Fill with adjustment. |
|---|---|---|---|
| reliminary)<br>eliminary)<br>(preliminary)<br>uperheated X for wet steam<br>ce area factor, A<br>height, I<br>hcy factor F <sub>1</sub><br>hcy factor Fε<br>hcy, η <sub>Z</sub>         | kJ/kg<br>kJ/kg<br>bar A<br>C for ti<br>m <sup>3</sup> /kg<br>mm       | 2480.1<br>2600.9<br>0.49<br>0.99<br>3.29<br>43<br>60.238<br>75  | =hi - $\Delta$ he, point Da<br>=he <sub>z</sub> + ( $\Delta$ he/z). Point Da-2<br>Point Da-2<br>See steam table for specific volume<br>Page 16<br>Equation 15 but replace P by ( $\Delta$ hs' x m x $\eta_{05}$ )<br>Fill with adjustment.  |
| eliminary)<br>(preliminary)<br>uperheated X for wet steam<br>ce area factor, A<br>height, I<br>hcy factor F <sub>1</sub><br>hcy factor Fε<br>hcy, ηz                                    | kJ/kg<br>kJ/kg<br>bar A<br>C for ti<br>m <sup>3</sup> /kg<br>mm       | 2480.1<br>2600.9<br>0.49<br>0.99<br>3.29<br>43<br>60.238<br>75  | =hi - $\Delta$ he, point Da<br>=he <sub>z</sub> + ( $\Delta$ he/z). Point Da-2<br>Point Da-2<br>See steam table for specific volume<br>Page 16<br>Equation 15 but replace P by ( $\Delta$ hs' x m x $\eta_{05}$ )<br>Fill with adjustment.  |
| (preliminary)<br>uperheated, X for wet steam<br>ce area factor, A<br>height, I<br>ncy factor $F_1$<br>ncy factor $F_2$<br>ncy, $\eta_Z$   | kJ/kg<br>bar A<br>C for ti<br>m <sup>3</sup> /kg<br>mm                | 2600.9<br>0.49<br>0.99<br>3.29<br>43<br>60.238<br>75  | =he <sub>z</sub> + ( $\Delta$ he/z). Point Da-2<br>Point Da-2<br>See steam table for specific volume<br>Page 16<br>Equation 15 but replace P by ( $\Delta$ hs' x m x $\eta_{05}$ )<br>Fill with adjustment.   |
| uperheated X for wet steam ce area factor, A height, I hey factor $F_1$ hey factor $F_2$ hey factor $F_2$ hey factor $F_2$  | bar A<br>C for ti<br>m <sup>3</sup> /kg<br>mm                         | 0.49<br>0.99<br>3.29<br>43<br>60.238<br>75  | Point Da-2<br>See steam table for specific volume<br>Page 16<br>Equation 15 but replace P by ( $\Delta$ hs' x m x $\eta_{05}$ )<br>Fill with adjustment.  |
| ce area factor, A<br>height, I<br>ncy factor $F_1$<br>ncy factor $F_8$<br>ncy, $\eta_Z$   | C for ti<br>m <sup>3</sup> /kg<br>mm                                  | 0.99<br>3.29<br>43<br>60.238<br>75  | See steam table for specific volume Page 16 Equation 15 but replace P by ( $\Delta$ hs' x m x $\eta_{05}$ ) Fill with adjustment.   |
| ce area factor, A<br>height, I<br>ncy factor $F_1$<br>ncy factor $F_8$<br>ncy, $\eta_Z$   | m <sup>3</sup> /kg<br>mm  | 3.29<br>43<br>60.238<br>75  | Page 16 Equation 15 but replace P by ( $\Delta$ hs' x m x $\eta_{05}$ ) Fill with adjustment.   |
| height, I<br>ncy factor F <sub>1</sub><br>ncy factor Fε<br>ncy, η <sub>Z</sub>  | mm  | 43<br>60.238<br>75  | Page 16 Equation 15 but replace P by ( $\Delta$ hs' x m x $\eta_{05}$ ) Fill with adjustment.   |
| height, I<br>ncy factor F <sub>1</sub><br>ncy factor Fε<br>ncy, η <sub>Z</sub>  |   | 60.238<br>75  | Equation 15 but replace P by ( $\Delta$ hs' x m x $\eta_{05}$ )<br>Fill with adjustment.  |
| ncy factor $F_1$<br>ncy factor $F_ε$<br>ncy, η <sub>Z</sub>   |   | 75  | Fill with adjustment.   |
| ncy factor $F_1$<br>ncy factor $F_ε$<br>ncy, η <sub>Z</sub>   | mm  |   |   |
| ncy factor F $\epsilon$   |   | 0.803   |   |
| ncy factor F $\epsilon$   |   |   | Max. 0.9 for Rateau turbine, fig. 16  |
| τς, η <sub>Z</sub>  |   | 1.00  | See fig. 13   |
| 5 1-  |   | 1.00  | See fig. 13   |
|   |   | 0.81  | $=\eta_{05} \mathbf{x} \mathbf{F}_{1} \mathbf{x} \mathbf{F} \mathbf{\epsilon}$  |
| partial, X  | 0   | 0.960   | Cas steam Mallian diaman  |
| st temperature, to  | C   | 51  | See steam Mollier diagram   |
| st specific volume, vo  | m <sup>3</sup> /kg  | 12.74   | See steam table   |
|   | kW  | 0.65  | Equation 5  |
| ge and Total  |   |   |   |
|   | kW  |   | $= z \times 0.5 \times (P_{LOSS-1} + P_{LOSS-Z})$   |
| e efficiency, $\eta_{AVG}$  |   | 0.76  | $=(\eta_1 + \eta_2) / 2$  |
|   | kJ/kg   | 2740  | See Mollier diagram   |
| ciency, η <sub>wετ</sub>  |   | 0.9989  | $h_{WET} = 2740 \text{ kJ/kg}$  |
| e efficiency, η   |   | 0.76  | $= \eta_{AVG} \ x \ \eta_{WET}$   |
| output, P   | kW  | 2998.2  | Equation 9  |
| nical efficiency, η <sub>m</sub>  |   | 0.963   | Figure 15   |
|   | kW  | 2887  | $= \eta_m x P$  |
|   | kJ/kg   | 2431  | $=$ hi - $\Delta$ hs' x $\eta$  |
|   | 2<br>2<br>2<br>2<br>2<br>2<br>2<br>2<br>2<br>2<br>2<br>2<br>2<br>2    | ssses, P <sub>LOSS</sub> kW<br>le efficiency, η <sub>AVG</sub><br>iciency, η <sub>WET</sub><br>e efficiency, η<br>output, P kW<br>nical efficiency, η <sub>m</sub><br>kW<br>kJ/kg | $\begin{array}{c ccccccccccccccccccccccccccccccccccc$   |

Power, kW

Page :



3



## STEAM TURBINE CALCULATION SHEET

| No.      | Designation                                |                    | Quantity    |             | Note and additional information                                 |
|----------|--|--------------------|-------------|-------------|---|
| 1<br>2   | Turbine type, figure 3                     |                    | RATEAU      | STAGES      |   |
| 3        | 51 - 5                                     |                    |             | URE TRUBINE |   |
| 4        | REQUIRED CONDITION                         |                    |             |             |   |
| 5        |  |                    | Normal      | Rated       |   |
| 6        | Driven equipment                           |                    | Air Com     | pressor     |   |
| 7        | Steam flow available                       | ton/hr             | 30          |             |   |
| 8<br>9   | N  | RPM                | 9000<br>110 |             |   |
| 9<br>10  | pi<br>ti                                   | bar A<br>C         | 650         |             |   |
| 11       | po   | bar A              | 5           |             |   |
| 12       | STEAM DATA                                 | bui / i            |             |             |   |
| 13       | hi   | kJ/kg              | 3737        |             | See steam Mollier diagram                                       |
| 14       | hos  | kJ/kg              | 2820        |             | See steam Mollier diagram                                       |
| 15       | Δhs  | kJ/kg              | 917         |             | = hi - hos  |
| 16       | Governor valve factor                      |                    | 0.97        |             | Multi valve 0.97, single valve 0.93                             |
| 17       | ∆hs'                                       | kJ/kg              | 889.49      |             | = Gov. vlv. Factor x $\Delta$ hs (equation 11)                  |
| 18       | hos'                                       | kJ/kg              | 2847.51     |             |   |
| 19       | pi'  | bar A              | 100         |             |   |
| 20       | ti'  | C                  | 645         |             | At hi and pi' (point B)   |
| 21       | vi'  | m <sup>3</sup> /kg | 0.0408      |             | See steam table at pi' and ti' (point B) or                     |
| 22       |  |                    |             |             | extrapolate in steam table                                      |
| 23       | CALCULATION                                |                    |             |             |   |
| 24       | Min. no. of stages, zmin                   |                    | 3           |             |   |
| 25       | Design dia., D                             | mm                 | 550         |             | Fig. 10. Nearest cross point RPM vs red dot line                |
| 26       | Calculated number of stages, z1            |                    | 5.63        |             | Eq. 12  |
| 27       | Design no. of stages, z                    | k l/ka             | 6           |             | Select with Integer number $= \Delta hs' / z$                   |
| 28       | Enthalpy per stage, $\Delta h_{STG}$       | kJ/kg              | 148.2       |             |   |
| 29<br>20 | Peripheral velocity, U                     | m/s                | 259.6       |             | Equation 1  |
| 30       | Head coefficient, $\mu_S$                  |                    | 2.20        |             | Equation 4  |
| 31       | Efficiency, $\eta_{05}$                    |                    | 0.83        |             | Figure 12   |
| 32       | Entrance area factor, A                    |                    | 34          |             |   |
| 33       | <u>First stage</u><br>Ι x ε                | <b>m</b> ==        | 1 400       |             | Equation 15 but raplace D by (Abely my rec)                     |
| 34<br>25 |  | mm                 | 1.493       |             | Equation 15 but replace P by ( $\Delta$ hs' x m x $\eta_{05}$ ) |
| 35<br>36 | Nozzle height, I<br>Degree of admission, ε | mm                 | 25<br>0.060 |             | Fill with adjustment<br>Max. 0.9 for Rateau turbine, fig. 16    |
|          | 5  |                    |             |             | •   |
| 37       | Efficiency factor F <sub>1</sub>           |                    | 0.97        |             | Figure 13   |
| 38       | Efficiency factor Fe                       |                    | 0.905       |             | Equation in figure 13   |
| 39       | Efficiency, η <sub>1</sub>                 | 1.14               | 0.73        |             | $= \eta_{05} \times F_1 \times F_{\varepsilon}$                 |
| 40       | hos <sub>1</sub>                           | kJ/kg              | 3588.75     |             | Make point at steam chart                                       |
| 41       | ∆he <sub>STG-1</sub>                       | kJ/kg              | 108.00      |             |   |
| 42       | he <sub>stg-1</sub>                        | kJ/kg              | 3629.00     |             | Make point at steam chart                                       |
| 43       | po <sub>1</sub>                            | bar A              | 65.0        |             | See steam chart   |
| 44       | to <sub>1</sub>                            | С                  | 590.0       |             |   |
| 45       | VO <sub>1</sub>                            | m <sup>3</sup> /kg | 0.059       |             | See steam table   |
| 46       | P <sub>LOSS-1</sub>                        | kW                 | 213.09      |             | Equation 5  |

| 1  |                                  |                    |        |  |
|----|----------------------------------|--------------------|--------|--|
| 2  | Last stage                       | "                  |        |  |
| 3  | ∆he                              | kJ/kg              | 648.0  | = $\eta x \Delta hs'$ (preliminary eff. = 1'stg eff.)<br>= hi- $\Delta he$ |
| 4  | hez                              | kJ/kg              | 3089.0 |  |
| 5  | hi <sub>stg-z</sub>              | kJ/kg              | 3197.0 | =he <sub>z</sub> + ( $\Delta$ he/z). Point Da-2                            |
| 6  | pi <sub>1</sub>                  | bar A              | 9.0    | See chart  |
| 7  | ti <sub>1</sub>                  | С                  | 375.0  |  |
| 8  | vi <sub>1</sub>                  | m <sup>3</sup> /kg | 0.33   |  |
| 9  | Entrance area factor, A          |                    | 43     |  |
| 10 | ΙΧε                              | mm                 | 11.506 | Equation 15 but replace P by ( $\Delta$ hs' x m x $\eta_{05}$ )            |
| 11 | Nozzle height, I                 | mm                 | 30     |  |
| 12 | 3                                |                    | 0.384  | Max. 0.9 for Rateau turbine, fig. 16                                       |
| 13 | Efficiency factor F <sub>1</sub> |                    | 0.96   | See fig. 13  |
| 14 | Efficiency factor F <sub>ε</sub> |                    | 0.99   | See fig. 13  |
| 15 | Efficiency, $\eta_Z$             |                    | 0.79   | $= \eta_{05} \times F_1 \times F_{\epsilon}$                               |
| 16 | P <sub>LOSS-Z</sub>              | kW                 | 30.98  | Equation 5   |
| 17 | Average and Total                |                    |        |  |
| 18 | Total losses, P <sub>LOSS</sub>  | kW                 | 732.23 | $= z \times 0.5 \times (P_{LOSS-1} + P_{LOSS-Z})$                          |
| 19 | Average efficiency, $\eta_{AVG}$ |                    | 0.76   | $=(\eta_1 + \eta_Z) / 2$   |
| 20 | Power output                     | kW                 | 4879   | Equation 9   |
| 21 | Mechanical efficiency, $\eta_m$  |                    | 0.977  | Figure 15  |
| 22 | BHP                              | kW                 | 4767   | $= \eta_m x P$   |
| 23 | he                               | kJ/kg              | 3064   |  |

